

In-situ characterization of gas-liquid precipitation reaction in a spray using rainbow refractometry*

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Abstract: Gas-liquid precipitation reactions in terms of a spray exist widely in energy, chemical, and environmental engineering. In this paper, a rainbow refractometry-based method is used to measure the reaction process of these spray-based gas-liquid precipitation reactions in a non-intrusive way. Rainbow refractometry can simultaneously provide information on thermochemical and physical properties of droplets. A global rainbow measurement system was built to characterize a CO₂ absorption reaction. Rainbow signals of spray droplets of Ca(OH)₂ solutions before and after CO₂ absorption were recorded and processed. Results indicated that the average refractive index of saturated H₂O-Ca(OH)₂ solution was 1.33569, which accorded with the Abbe measurement. After the absorption reaction, the refractive index of droplets decreased to 1.33517 which is close to that of water. The reaction extent was therefore reflected in the change of the refractive index of droplets. An extra experiment of CO₂ absorbed by Ba(OH)₂ solutions was conducted. The refractive index of droplets decreased with the reaction process, which acted well as an evolution indicator of the reaction. A heat transfer analysis of the reaction was also carried out. Due to the high heat dissipation performance of fine droplets, the temperature increase in the measurement volume was estimated to be less than 0.61 K, which has almost no effect on the measured results. The rainbow refractometry-based method shows good potential for in-situ characterization of a gas-liquid precipitation reaction.

Key words: Rainbow refractometry; In-situ characterization; Refractive index; Gas-liquid precipitation reaction
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1 Introduction

Environmental issues, such as haze weather and global warming, are becoming a major concern for the public. Excessive SO_x and NO_x, mainly produced

by the burning of fossil fuels, are two causes of haze formation. Nontoxic CO₂ is the major source of greenhouse gases (GHG) believed to cause global warming and represents 76.7% of GHG. Recently, China committed to promoting the ultra-low emissions of coal-fired power plants. Wet flue gas desulfurization (WFGD) (Gao et al., 2008, 2009) and CO₂ capture by monoethanolamine are two ways of pollutant and emission control, which all involve the gas-liquid absorption reaction. WFGD has been used as a leading technology for many years in the field of wet desulfurization and denitrification in a power plant. The slurry droplets of lime used as the desulfurization or denitrifying agent have a chemical

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absorption precipitation reaction with SO_2 or NO_x during the atomization. They ultimately appear in the form of droplets with solid inclusion in the air. Therefore, in-situ characterization of the evolution of the gas-liquid absorption precipitation reaction is beneficial for monitoring and improving the removal efficiency of pollutants.

So far, few studies have focused on the in-situ characterization of the gas-liquid absorption precipitation reaction. As an advanced optical diagnostic method, rainbow refractometry is a potential technique for the measurement of refractive index (RI) and size distribution of spray droplets by recording and analyzing the elastic scattering light around the rainbow angle in real time. The standard rainbow technique (SRT) for measuring a single droplet or identical droplets was first proposed by Roth et al. (1990). In order to overcome the problems of ripple structures and non-spherical droplets, van Beeck et al. (1999) invented a global rainbow technique (GRT) for measuring the mean RI and size distribution of polydispersed droplets by extending the exposure time and enlarging the aperture. Wu et al. (2014) presented a 1D rainbow refractometry which simultaneously obtains parameters of droplets on a line, and rainbow refractometry was extended to a 1D measurement technique. Rainbow refractometry (Wu et al., 2017) has achieved great popularity in measuring concentration (Zhao and Qiu, 2006; Wilms and Weigand, 2007; Wu et al., 2012), non-sphericity (van Beeck and Riethmuller, 1996; Lohner et al., 1999; Saengkaew et al., 2009; Yu et al., 2013a, 2013b), RI gradient (Saengkaew et al., 2007; Rosebrock et al., 2016; Song et al., 2016; Li et al., 2017), droplet diameter variations at the nanoscale as well as recently in the diagnostic of spray evaporation (Promvongsa et al., 2017) or combustion (Letty et al., 2013; Verdier et al., 2016) and pollutant removal (Ouboukhlik et al., 2015a, 2015b).

This paper investigates the in-situ characterization of the gas-liquid absorption precipitation reaction using rainbow refractometry for the first time. In this study, the measurement theories, including the principle of rainbow refractometry and parameter inversion, are introduced first, followed by the presentation of the experimental setup. Then, the signal processing and heat transfer are provided.

2 Measurement theories

2.1 Principle of rainbow refractometry

The path of light reflected and refracted at the equatorial plane of a droplet is shown in Fig. 1, where P is the Debye series, D is the droplet diameter, and α_r is the refractive angle. From geometrical optics and Snell's law, the scattering angle is given by

$$\theta = \pi + 2\alpha - 4 \arcsin\left(\frac{\sin \alpha}{m}\right), \quad (1)$$

where θ denotes the scattering angle, α denotes the incident angle, and m denotes the relative RI of liquid to air. According to Eq. (1), a minimum named the geometrical rainbow angle exists at a specific incident angle. The geometrical rainbow angle θ_{rg} is expressed as

$$\theta_{rg} = 2 \arccos \left[\frac{1}{m^2} \left(\frac{4 - m^2}{3} \right)^{3/2} \right]. \quad (2)$$

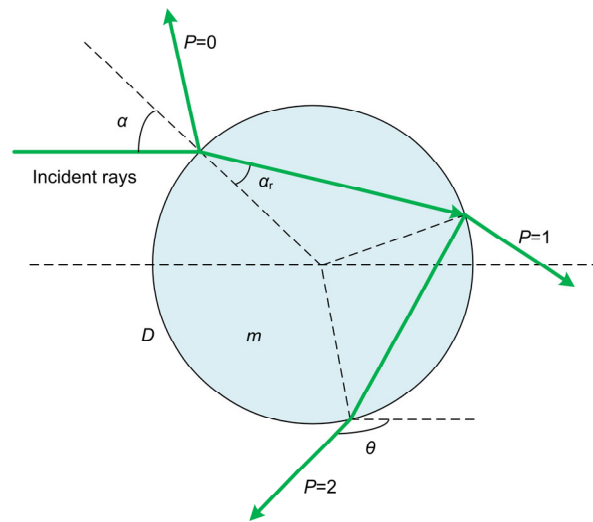


Fig. 1 Path of light reflected and refracted at the equatorial plane of a droplet

The geometrical rainbow angle θ_{rg} from Eq. (2) significantly depends on the RI of liquid (m). Although there are some deviations, the RI can be obtained from the angular location of the rainbow. The change in droplet size leads to a variation in angular spacing of the rainbow fringes. Thus, the

physical and thermochemical parameters of droplets can be determined from the intensity distribution of the rainbow.

2.2 Parameter inversion

The global rainbow signal of spray droplets is processed by the independent inversion algorithm proposed by Saengkaew (2005). The RI and size distribution are obtained by solving the equation using the non-negative least-squares algorithm:

$$I_g = \begin{bmatrix} I_g(\theta_1) \\ I_g(\theta_2) \\ \vdots \\ I_g(\theta_j) \end{bmatrix} = \begin{bmatrix} I(d_1, \theta_1, m), I(d_2, \theta_1, m), \dots, I(d_i, \theta_1, m) \\ I(d_1, \theta_2, m), I(d_2, \theta_2, m), \dots, I(d_i, \theta_2, m) \\ \vdots \\ I(d_1, \theta_j, m), I(d_2, \theta_j, m), \dots, I(d_i, \theta_j, m) \end{bmatrix} \cdot \begin{bmatrix} N(d_1) \\ N(d_2) \\ \vdots \\ N(d_i) \end{bmatrix} = \mathbf{T} \cdot \mathbf{N}, \quad (3)$$

where $I_g(\theta_j)$ is the total light intensity of the global rainbow at the scattering angle θ_j ; $I(d_i, \theta_j, m)$ is the rainbow light intensity at the scattering angle θ_j for a droplet with an RI of m and diameter of d_i , which forms the rainbow coefficient matrix \mathbf{T} ; $N(d_i)$ is the number of droplets with diameter d_i , and this forms the size distribution \mathbf{N} .

The light intensity-angle distribution of global rainbow I_g is recorded by an array CCD camera. Initial RI and size distribution are obtained from an initial estimation by solving the equation using the non-negative least-squares algorithm. The RI m and size distribution \mathbf{N} are optimized by iteratively searching for the minimum absolute error of the recorded rainbow signal and the fitted rainbow signal using Brent's method. The fitted rainbow signal is computed using the modified Nussenzveig theory with correction coefficients (Saengkaew et al., 2006). This theory takes into account the interference be-

tween the light experiencing one internal reflection ($P=2$) and the ripple structure (external reflected light ($P=0$) interference with one internal refracted light). Eq. (4) (Nussenzveig, 1969) indicates the theoretical calculations of the one internal refracted light around the rainbow angle.

$$f_{\text{rainbow}}(x, \theta) = -\frac{D}{2} \cdot \frac{16 \exp\left(-\frac{i\pi}{4}\right)}{27\sqrt{3}} \cdot \sqrt{\frac{\pi}{\sin\theta}} \cdot c \cdot (6sx)^{\frac{1}{6}} \cdot \exp\left(6icx + is\epsilon x + iA\epsilon^2 x + O(x\epsilon^2)\right) \cdot \left\{ A_i \left[1 + O(\epsilon) + O(x^{-1}) \right] \left[\frac{(2x)^{2/3} c\epsilon}{(3s)^{1/3}} (1 + B\epsilon + O(\epsilon^2)) \right] + \frac{iCA'_i}{(2x)^{1/3}} \left[-\frac{(2x)^{2/3} c\epsilon}{(3s)^{1/3}} (1 + B\epsilon + O(x\epsilon^2)) \right] \right\}, \quad (4)$$

where $x = \pi D/\lambda$ is the dimensionless size parameter, λ is the wavelength, $\epsilon = \theta - \theta_{\text{rg}}$ is the relative scattering angle, f_{rainbow} is the rainbow amplitude, O is infinitesimal asymptotic, A_i is the Airy function, A'_i is the derivative of A_i , and A , B , C , c , and s are the coefficients which only depend on the RI.

3 Experimental set up

An in-situ global rainbow experimental measurement system was built to characterize the evolution of the absorption of CO_2 by the $\text{H}_2\text{O}-\text{Ca}(\text{OH})_2$ solution, and the schematic is shown in Fig. 2. A CO_2 jet was arranged in a vessel made of Plexiglas with a saturated $\text{H}_2\text{O}-\text{Ca}(\text{OH})_2$ solution spray above the vessel. The measurement objects were spray droplets of a saturated $\text{H}_2\text{O}-\text{Ca}(\text{OH})_2$ solution before the absorption reaction, and droplets of a $\text{H}_2\text{O}-\text{CaCO}_3$ suspension after the absorption. The experimental system comprised a spray generating system and an optical system.

The spray was generated by an ultrasonic nozzle (model YPWH32020L, frequency 20 kHz). A pump provided the necessary pressure (101–1010 kPa) for the transport of the measured liquid from the sample pool. The nozzle was placed on the top of the vessel, and created a spray with a mean droplet diameter of 60 μm and a mean velocity of about 1.2 m/s (for a

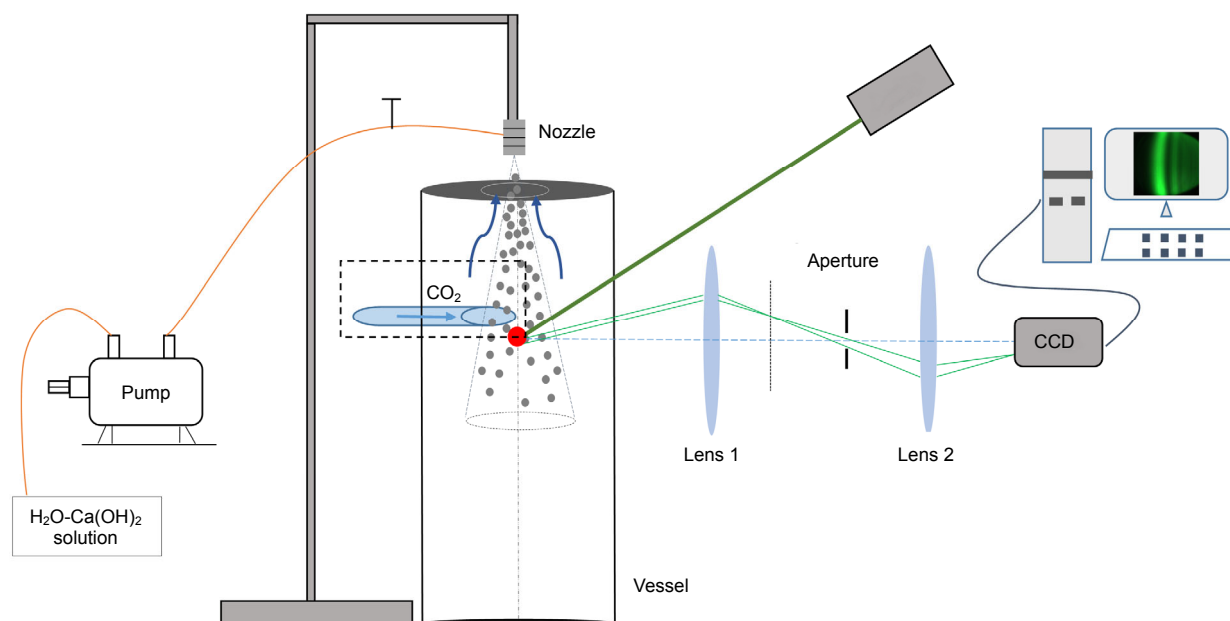


Fig. 2 Schematic of global rainbow experimental measurement system for characterization of CO_2 absorption reaction

pump flow rate of 180 ml/min). The measurement volume was located at the spray center, about 40 cm from the nozzle orifice. The CO_2 gas inlet, with a flow rate of 90 ml/min, was located around the measurement volume. This brought the gas and liquid into counter current exchange.

The optical system consisted of an optical platform, a single longitudinal mode laser (power=200 mW, $\lambda=532$ nm) with coherence length of 50 m, a CCD camera (resolution 2048×2048 pixels, pixel size: $7.4 \mu\text{m}/\text{pixel}$), two plano-convex lenses (diameter=10 cm, focal length $f=16$ cm), an aperture, and a computer used to record and process the rainbow signals. The measurement volume was illuminated by a vertical polarized laser beam with a polarization ratio of 100. Scattering light around the rainbow angle of the droplets ($P=2$, about 132° – 147°) was collected by the first lens. Located in the image plane of the measurement volume in lens 1, the aperture could effectively eliminate stray environmental light and control the measurement volume. The second lens conjugated the back focal plane of the first lens on the CCD. The scattering light at each scattering angle was recorded by different columns in the CCD. The two spherical lenses and one aperture, together with the CCD, form the global rainbow imaging system. The working distance (namely, distance from the measurement volume to lens 1) was 24 cm, and the

aperture size was about 2 mm. The exposure time of the CCD camera with a tunable range of $20 \mu\text{s}$ – 100 ms was fixed at 50 ms to record numerous superimposed rainbows on each frame. In addition, the relationship of scattering angle with CCD pixel was calibrated using a linear fitting method by a reflector mirror with a rotating accuracy 0.033° .

4 Results and discussion

4.1 Rainbow signals process and analysis

The RI of $\text{Ca}(\text{OH})_2$ solutions at different mass fractions was measured by an Abbe refractometer (model 2WAJ) as a standard. Since the solubility of $\text{Ca}(\text{OH})_2$ in 100 ml water is about 0.16 g at room temperature, $\text{Ca}(\text{OH})_2$ solutions with mass fractions of 0%, 0.08%, and 0.16% were prepared using de-ionized water and $\text{Ca}(\text{OH})_2$ powder and a microbalance. The room temperature, which also affected the RI, was about 24.2°C measured by a K-type thermocouple.

It must be noted that the wavelength used in the Abbe refractometer was 589.3 nm which differed from 532 nm used in this experiment. Therefore, it is necessary to convert the results from 589.3 nm to 532 nm. The equation for the water RI as a function of wavelength and temperature has already been fully

studied, as given by Eq. (5) (Quan and Fry, 1995), and the converted results are also shown in Fig. 3. The deviation of RI introduced by the wavelength difference is equal to 2.0×10^{-3} under a temperature from 0 °C to 20 °C, illustrated in Fig. 3. The RI is significantly proportional to the mass fraction. The RI of the saturated $\text{H}_2\text{O}-\text{Ca}(\text{OH})_2$ solution is about 1.3356, while that of water is about 1.3352. This preliminary experiment illustrated that there was obviously a corresponding relationship between the concentration of $\text{Ca}(\text{OH})_2$ solutions and the RI.

$$\begin{aligned}
 n_T^\lambda &= 1.31405 - 2.02 \times 10^{-6} T^2 \\
 &+ (15.868 - 0.00423T)\lambda^{-1} \\
 &- 4382\lambda^{-2} + 1.1455 \times 10^6 \lambda^{-3}, \\
 n_T^{532} - n_T^{589.3} &= (20.46106762 - 7.731200136 \times 10^{-3} T) \times 10^{-4} \\
 &\approx 2 \times 10^{-3},
 \end{aligned}
 \tag{5}$$

where T denotes the temperature, and n_T is the RI at temperature T .

As shown in Fig. 4a, the global rainbow signals of the atomized droplets before and after CO_2 absorption were recorded, and the products were sampled and analyzed using an off-line microscope. It could be seen from the micrograph that lots of small CaCO_3 solid particles of size 1–3 μm appear after the absorption reaction. The number concentration of CaCO_3 particles with a mean size of 2 μm is around 23 in a droplet. The intensity curves of the rainbow signals before and after CO_2 absorption are shown in

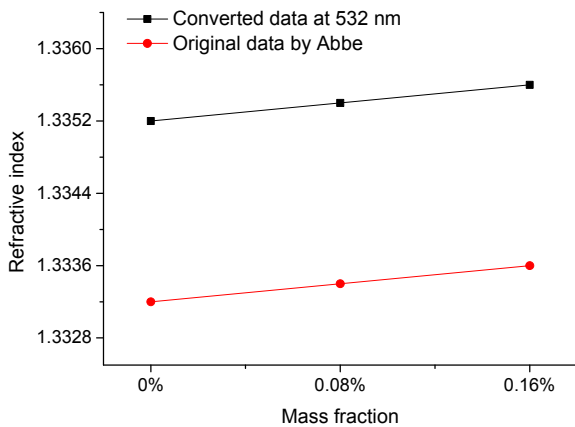
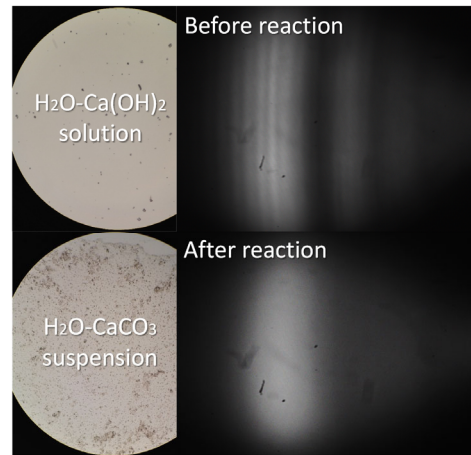
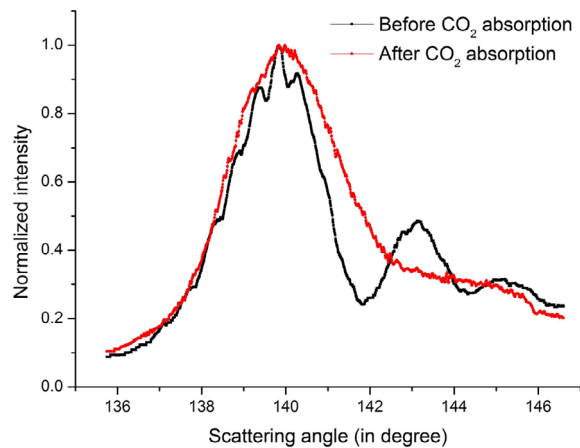


Fig. 3 Refractive index of $\text{Ca}(\text{OH})_2$ solutions at different mass fractions

Fig. 4b. The absorption of CO_2 brings about a significant leftward shift in the increase part of the main peak. Due to the reduction of droplet diameter (about 8 μm), there exists a larger peak width for the rainbow signal after the reaction. The results of GRT indicate that the average RI of saturated $\text{H}_2\text{O}-\text{Ca}(\text{OH})_2$ solution is 1.33569 ($\lambda=532 \text{ nm}$), which is consistent with Fig. 3. After absorption, the $\text{Ca}(\text{OH})_2$ dissolved in the water is converted into insoluble CaCO_3 particles, and the average RI of the droplets decreases to 1.33517, which is close to that of the deionized water calculated by Eq. (5). The measured RI for each condition was averaged from 30 rainbow signals, and the error bars were about 1.0×10^{-4} .



(a)



(b)

Fig. 4 Rainbow signals for $\text{H}_2\text{O}-\text{Ca}(\text{OH})_2$ solution before and after CO_2 absorption (a) and intensity curves of the rainbow signals (b)

The chemical equation between $\text{Ca}(\text{OH})_2$ and CO_2 is shown in Eq. (6). With the process of reaction, the concentration of $\text{Ca}(\text{OH})_2$ falls with an increase in that of CaCO_3 , while the total molarity is fixed. Based on the conclusions of our previous work, the solid inclusions ($\leq 4 \mu\text{m}$) at low concentrations have no effect on the measurement of the liquid RI. Small CaCO_3 solid particles as inclusions in the host droplet will obstruct some scattering rays, causing some disturbances on the primary and supernumerary bow. These disturbances to the rainbow pattern depend on the position, particle size, and number concentration of the inclusions. In the case of recording multiple droplets with inclusions at low concentration using GRT, the disturbances would be superimposed like the ripple structure and not affect the parametric measurement of the liquid phase. As illustrated in Fig. 5, the RI variances caused by different mass concentrations ($C_m < 6.92\%$) are about 2.0×10^{-4} . The RI of droplets decreases with the reaction process, and the amount of the reaction could be reflected in the shift of the rainbow angular location (i.e. RI of droplets). Therefore, the process of the precipitation reaction can be observed and analyzed by the in-situ measurement of GRT.

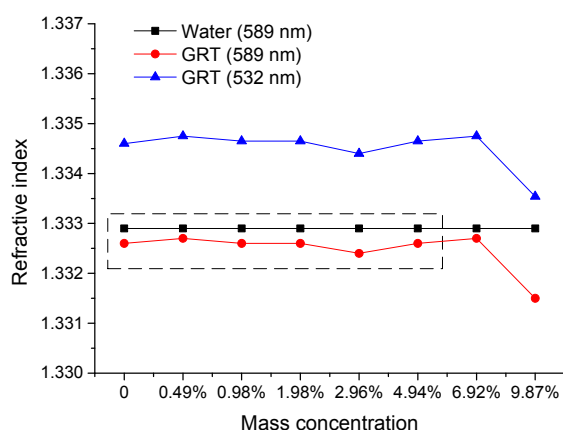
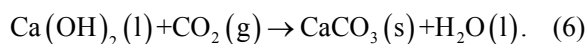


Fig. 5 Refractive index of droplets of $\text{H}_2\text{O}-\text{CaCO}_3$ suspensions ($C_m=0\%-9.87\%$) using GRT

The reaction rate, which is critical to the reaction, is limited by the concentration of reactants and mass transfer efficiency of diffusion and absorption. Traditional experimental study of the reaction rate is

of that in the reactor. A certain concentration of $\text{H}_2\text{O}-\text{Ca}(\text{OH})_2$ solution contained in a vessel reacts with CO_2 gas from pressure cylinders. The stirrer at the bottom of the reactor continuously stirs at a constant rate to speed up the reaction. The average reaction rate for saturated $\text{H}_2\text{O}-\text{Ca}(\text{OH})_2$ solution in the literature is about 0.07 g/s (Haghnegahdar et al., 2011). Since the atomized droplet provides a larger surface area for contacting the reactants, heat transfer, mass transfer, and the chemical reaction occur simultaneously. When the liquid reacts with CO_2 in the form of atomized droplets, the reaction speed can be greatly increased, and the absorption efficiency can be improved. In this experiment, the liquid flow rate was 3 ml/s, and the solubility of $\text{Ca}(\text{OH})_2$ at room temperature is 0.00166 g/ml. The reaction between injected spray droplets and CO_2 takes less than 71.1 ms which is short enough to be assumed as an instantaneous process. Therefore, the concentration gradient of the reactant in the measurement volume can be ignored.

$\text{Ba}(\text{OH})_2$ solutions were also selected to absorb CO_2 , due to their greater solubility (27 times more than that of $\text{Ca}(\text{OH})_2$). CO_2 at different flow rates (0, 2, 4, 6, 8, 10, and 12 ml/s) was pumped to react with $\text{Ba}(\text{OH})_2$ solutions ($C_m=3.0\%$), and these represent different reaction processes. The rainbow signals and the micrographs at the seven working conditions were recorded and processed, as shown in Fig. 6. Because of the scattering extinction introduced by an increasing number of generated solid particles, absolute light intensities of rainbow signals become smaller with the reaction process.

The off-line micrographs show that the small solid particles increase with the reaction process. In addition, RI has a one-to-one relationship with the micro-morphology of droplets, which in-situ reveals the reaction process. With the decrease of RI, the concentration of solid particles increases, which fits well with the results of the Abbe refractometer.

4.2 Heat transfer analysis

According to the position of the measurement volume and the velocity of the droplets, the contact time Δt is about 333 ms. During this time, there is in total $m_w=1.0 \times 10^{-3}$ kg $\text{Ca}(\text{OH})_2$ (aq) ($C_m=0.16\%$) injected from the nozzle, which is selected as the study object. The molecular weight of Calcium hydroxide is

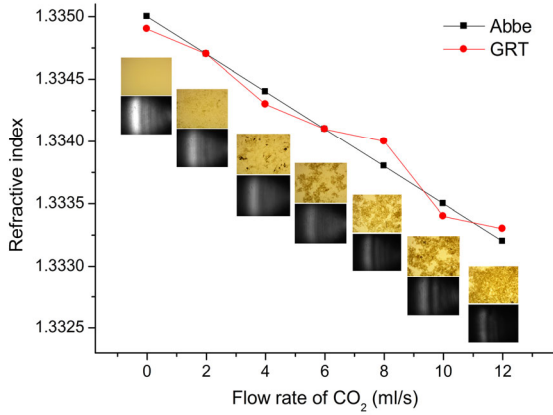


Fig. 6 Rainbow characterization of CO₂ absorption reaction in different processes (Abbe means the RI measured by Abbe refractometer)

74 g/mol. The chemical reaction enthalpy of Eq. (6) is about $\Delta H = -97.3$ kJ/mol (298.15 K) (Zumdahl, 2009), and thus the heat release Q_r of the reaction is 2.1 J. The specific heat capacity of the aqueous solution is approximately equal to that of water, $C_v = 4.2$ kJ/(kg·K).

The heat transfer between a droplet in the falling state and air could be classified as forced convection heat transfer for flow in a single sphere, and the coefficient h is calculated by the following equations:

$$Nu = 2 + \left(0.4Re^{1/2} + 0.06Re^{2/3}\right) Pr^{0.4} \left(\frac{\eta_\infty}{\eta_w}\right)^{1/4}, \quad (7)$$

$$Re = \frac{VD}{\nu}, \quad (8)$$

$$h = Nu \cdot \frac{\lambda_c}{D}, \quad (9)$$

where Nu denotes the Nusselt number, Re denotes the Reynolds number, Pr denotes the Prandtl number of air ($Pr = 0.70856$), η_∞ is the kinetic viscosity coefficient of air at room temperature ($\eta_\infty = 1.82148 \times 10^{-5}$ kg/(m·s)), η_w is that at the droplet temperature ($\eta_w = 1.8462 \times 10^{-5}$ kg/(m·s)). The qualitative temperature is room temperature ($T_\infty = 298.15$ K), and characteristic length is the droplet diameter ($D = 60$ μm). In addition, Eq. (7) (Whitaker, 1972) is valid in two ways: $0.71 < Pr < 380$, and $3.5 < Re < 76000$. In Eq. (8), V is the air velocity ($V = 1.2$ m/s), and ν is the kinematic viscosity coefficient of air ($\nu = 1.5617 \times 10^{-5}$ m²/s). In Eq. (9), λ_c is the thermal conductivity of air ($\lambda_c = 0.025854$ W/(m·K)).

Based on the above formulas and input parameters, $Re = 4.61$, $Nu = 2.89$, and thus $h = 1245$ W/(m²·K).

The heat transfer equation is expressed as:

$$Q_r - Q_d = C_v m_w \Delta T, \quad (10)$$

$$Q_d = h \cdot A_s \cdot \overline{\Delta T} \cdot \Delta t, \quad (11)$$

$$A_s = N \cdot 4\pi d^2 = \frac{m_w}{\rho \frac{4}{3}\pi d^3} \cdot 4\pi d^2 = \frac{3m_w}{\rho d}, \quad (12)$$

$$\Delta T < \frac{Q_r}{\left(C_v m_w + h \frac{3m_w}{\rho d} \Delta t\right)}, \quad (13)$$

where Q_d is the heat dissipation, A_s is the total liquid superficial area, ρ is the aqueous density ($\rho = 1000$ kg/m³), d is the droplet radius ($d = 30$ μm), N is the droplet number of the study object, $\Delta T = T_{\text{droplet}} - T_\infty$ is the temperature difference between the droplets and the test environment, and $\overline{\Delta T}$ is the time mean temperature difference (absolutely $\overline{\Delta T} > \Delta T$). On the basis of the above equations and parameters, ΔT is estimated to be less than 0.05 K.

Considering the convection heat transfer between the droplets and the test environment, the temperature increase is less than 0.05 K. The heat transfer of reaction between Ba(OH)₂ solutions and CO₂ can be analyzed in the same way, with a maximum ΔT of less than 0.61 K.

The reaction heat, which depends on the concentration of the measured aqueous droplets, will lead to a ΔT , influencing the RI indirectly. From careful estimation, ΔT from the first reaction is less than 0.05 K, and ΔT from the second reaction is less than 0.61 K. In this case, the maximum RI variation for water is less than 6.0×10^{-5} which is within the measurement accuracy of rainbow refractometry. Therefore, the effect from the temperature increase on the results can be ignored, and the same applies to the temperature gradient.

5 Conclusions

Rainbow refractometry was used to measure the reaction process of a gas-liquid absorption precipitation reaction. Measurement theories, including the

principle of rainbow refractometry and parameters inversion, were introduced. A global rainbow experimental measurement system was built for in-situ characterization of the CO₂ absorption reaction. A preliminary experiment illustrated the feasibility of characterization of the concentration of Ca(OH)₂ solutions by refractive index. The rainbow signals of spray droplets of Ca(OH)₂ solution before and after CO₂ absorption were recorded and processed. The results of GRT indicated that the average refractive index of saturated H₂O-Ca(OH)₂ solution was 1.33569, which accorded with Abbe measurement. After the reaction, the refractive index of droplets decreased to 1.33517 which was close to that of water. The reaction extent was reflected in the shift of the rainbow angular location (i.e. refractive index of droplets). Pumping different flow rates of CO₂, an extra experiment on CO₂ absorbed by Ba(OH)₂ solution at different processes was conducted. The refractive index decreased as the reaction proceeded, which acted well as an evolution indicator of the reaction. The heat transfer of the absorption reaction was also analyzed based on a flow in single sphere model. After careful analysis, the temperature increase in the measurement volume was estimated to be less than 0.61 K, which was within the measurement accuracy of rainbow refractometry and could be ignored.

The feasibility of the preliminary investigation had been verified. All these results provide a new insight on the in-situ measurement of the gas-liquid precipitation reaction. The next step in our research will be to investigate the reaction rate and mass transfer for further control and optimization.

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中文概要

题目: 彩虹折射法对喷雾气液沉淀反应的原位表征

目的: 喷雾气液吸收化学反应广泛存在于能源、化学和环境工程中。比如在能源环境领域，湿法烟气脱硫(WFGD)中的碱性喷雾吸收脱除气体污染物，乙醇胺(MEA)吸收脱除CO₂酸性气体。对这类反应的表征，有利于控制和改善污染物脱除效率。本文尝试利用气液吸收沉淀反应过程中液滴折射率的变化来原位表征反应进程。

创新点: 1. 基于彩虹折射法，首次对气液吸收沉淀反应的原位表征进行探究；2. 通过若干实验和详细的传热计算分析，成功验证了其可行性和有效性。

方法: 1. 通过与 Abbe 折射仪对比，确定全场彩虹测量的准确性(图 3 和公式(5))；2. 搭建全局彩虹技术(GRT)测量系统进行喷雾测量实验(图 2)，并记录反应过程中的彩虹图像和离线采样液滴用于显微分析(图 4 和 5)；3. 对涉及到的气液吸收沉淀反应进行传热计算和分析(公式(7)~(13))。

结论: 1. 初步表明了利用溶液折射率表征Ca(OH)₂质量分数的可行性。2. 实验结果表明GRT的测量结果精确；反应后液滴折射率减少并趋向于水，反应进程可体现在彩虹角(即折射率)的变化上。3. 不同浓度Ba(OH)₂吸收CO₂的反应进一步证明了该方法原位表征气液吸收沉淀反应的可行性。4. 反应的传热计算和分析表明反应热所造成的温度升高可以忽略，验证了该方法的有效性。

关键词: 彩虹折射法；原位表征；折射率；气液吸收沉淀反应